

Subcall-Oriented Modelling of Overload Control in SPC Switching Systems

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ABSTRACT

The performance of stored program controlled (SPC) switching systems is strongly influenced by their subcall handling efficiency, especially in overload situations. The subcall generation and handling process depends mainly on the interaction between the actual system effectiveness and the customer behaviour. In this paper overload control aspects in SPC switching systems are investigated by means of two subcall-oriented queueing models.

In the first model the subcall and call handling processes are considered together, whereby an overload control strategy, the bad-call-interruption scheme (BCI), is presented and investigated. The interdependency between the subcall generation process, the call completion characteristics and the call waiting time according to the customer behaviour, is pointed out in the second model. A state-dependent call throttling method is analyzed, whereby the instationary system reaction on time varying overload traffic patterns and the instationary performance of the overload control scheme are investigated.

1. INTRODUCTION

In modern stored program controlled switching systems, a modular structure is often provided for both hard- and software. The system functions are divided and allocated among a number of autonomous processors and processes. Due to the modular structure the number of tasks or telephonic events (*subcalls*) generated per call attempt is larger in comparison with conventional, centralized controlled SPC switching systems. Thus, the overall performance of the switching system is strongly influenced by the subcall handling efforts, which become a critical factor in overload situations.

Subcall-oriented performance considerations in telephone switching systems are given in a number of papers [3-6]. Basic models for overload control mechanisms are discussed in [2, 6] and [12]. Detailed descriptions of subcall traffic are considered in [4, 5] and [11], where simulation studies are presented. Several aspects concerning the modelling of SPC switching system are outlined in [3].

The subcall-oriented modelling technique offers an appropriate tool for performance investigations in SPC switching systems. By means of this method, the call handling process can be modelled and investigated in more detail, where the system behaviour in overload situations and the effectiveness of overload control strategies can be realistically investigated. Furthermore, to account for the observed subcall generation process with respect to subscriber behaviour, models describing the interdependency between the call waiting time, the subcall traffic and the call completion rate can be developed.

2. COMPOUND MODEL FOR CALL AND SUBCALL HANDLING

2.1 Modelling approach and overload control strategy

The subcall traffic characteristics in a SPC switching system is strongly affected by the call arrival and handling process. In order to model this influence in detail, both the call and subcall processes must be taken into account. By means of the compound model for call and subcall handling developed in this chapter, the dependency of the call completion characteristics on the subcall handling efficiency will be investigated.

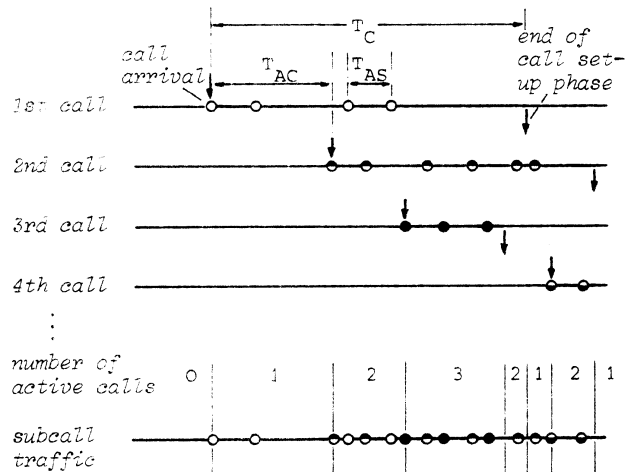


Fig. 2.1 Subcall generation and superposition in switching systems

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Fig. 2.1 illustrates the generation and the superposition of subcalls as well as the relationship between call and subcall traffic streams. It can be clearly seen here that the subcall stream constitutes a non-recurrent process. Its intensity is modulated by the number of active calls in the system.

The random variable (r.v.) T_{AC} stands for the interarrival time of calls, which follow a Poisson process with the rate λ . Considering the fact that the most subcalls are produced during the set-up phase T_C of a call, this phase will be used in the model as the main subcall producing phase. Taking into account the mixture of call types in a switching system, (e.g. successful or abandoned calls, facilities calls,...) the r.v. T_C is assumed to be negative exponentially distributed. The intervals between generated subcalls, which belong to a call, are characterized by the independently identically distributed r.v. T_{AS} . Because of the large number of subcalls produced per call in SPC switching systems and considering the different types of subcalls produced by different call controlling processes (call handling, signalling, device handling, etc...), T_{AS} is assumed to be negative exponentially distributed. Thus, the subcall process corresponding to an active call is characterized by a Poisson process with the rate λ_C .

The compound model for call and subcall handling is depicted in Fig. 2.2. An accepted call request activates a subcall source (subcall generator), which produces subcalls with the rate λ_S during the call set-up phase. After this time, corresponding to the r.v. T_C mentioned above, the subcall source will be idled. According to the call handling capacity of the switching system, the number of subcall sources is limited by n .

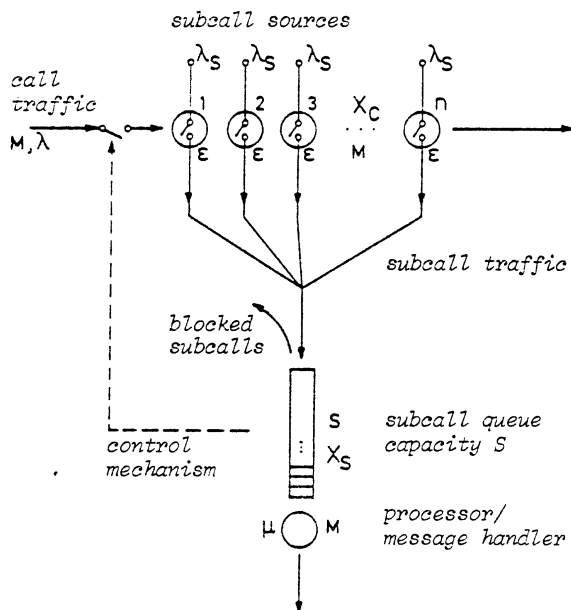


Fig.2.2 Compound model for call and subcall handling

Subcalls generated by active sources are superposed and form the subcall traffic stream offered to the subcall handler, which models the processor or the control unit. The subcall queue has the finite capacity S . Taking into account all subcall types requiring different processing times, the subcall handler is approximated to be a Markovian server with the mean service time $1/\mu$.

When the subcall queue is completely filled, further subcalls offered will be considered as blocked. A call which has produced a blocked subcall cannot be completed and is said to become a *bad-call*. The performance of the switching system will be degraded by bad-calls, since the subcall handler has spent an ineffective amount of processing time to handle subcalls belonging to bad-calls. Furthermore, according to signalling delays and customer reactions, a bad-call will produce further ineffective subcalls. These effects reduce in a dramatic way the system performance in overload situations.

The considerations discussed above lead to an overload control mechanism, the *bad-call-interruption* method (BCI), which allows a more effective use of the system real-time capacity. In accordance with the BCI strategy, a call is cleared immediately after producing a blocked subcall. This scheme can be implemented by hard- or software, e.g. by means of an instantaneous changing of the event scanning process for active calls. The aim of the BCI strategy is a reservation of processor capacity to handle completable calls (good-calls), in order to optimize the call completion rate of the switching system.

2.2 Analysis

The actual system state can be described by means of the two r.v. X_C and X_S , which represent the actual number of calls and subcalls in the system, respectively. According to the memoryless property of the model components, the analysis can be done by means of a two-dimensional Markov process, using standard techniques of queueing theory [1].

With the state probabilities

$$P(i, j) = \Pr\{X_C = i, X_S = j\}, i=0, \dots, S+1, j=0, \dots, n, \quad (2.1)$$

the corresponding state transition diagram can be developed as shown in Fig. 2.3. In this diagram, Θ is an auxiliary variable indicating the presence of the BCI overload control strategy, where the values $\Theta=1$ and $\Theta=0$ stand for the two cases with and without bad-call-interruption, respectively.

According to the state transition diagram, a set of difference equations for the steady state is derived, with which the state probabilities are numerically calculated using an iteration method with overrelaxation (see [12]).

The mean number E_C of calls and E_S of subcalls in system can be determined by :

$$E_C = \sum_{i=0}^{S+1} \sum_{j=0}^n j \cdot P(i, j), \quad (2.2a)$$

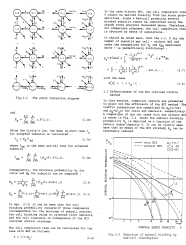


Figure 1: [Description of the figure content]

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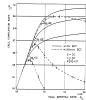


Fig. 1. Dependence of the rate of polymerization on the concentration of the initiator.

The curves in Fig. 1 are calculated for the following values of the rate constants: $k_1 = 10^4$, $k_2 = 10^3$, $k_3 = 10^2$, $k_4 = 10^1$, $k_5 = 10^0$, $k_6 = 10^{-1}$, $k_7 = 10^{-2}$, $k_8 = 10^{-3}$, $k_9 = 10^{-4}$, $k_{10} = 10^{-5}$, $k_{11} = 10^{-6}$, $k_{12} = 10^{-7}$, $k_{13} = 10^{-8}$, $k_{14} = 10^{-9}$, $k_{15} = 10^{-10}$.

1. INITIAL STAGE OF POLYMERIZATION

In the initial stage of polymerization, the concentration of the initiator is high and the concentration of the radical is low. The rate of polymerization is determined by the rate of initiation.

The rate of initiation is given by the equation:

$$R_i = k_1 I_0$$

where R_i is the rate of initiation, I_0 is the concentration of the initiator, and k_1 is the rate constant of initiation.

The rate of polymerization is given by the equation:

$$R_p = k_2 M_0$$

where R_p is the rate of polymerization, M_0 is the concentration of the monomer, and k_2 is the rate constant of propagation.

The rate of termination is given by the equation:

$$R_t = k_3 M_0^2$$

where R_t is the rate of termination, M_0 is the concentration of the monomer, and k_3 is the rate constant of termination.

The rate of chain transfer is given by the equation:

$$R_{ct} = k_4 M_0$$

where R_{ct} is the rate of chain transfer, M_0 is the concentration of the monomer, and k_4 is the rate constant of chain transfer.

The rate of depropagation is given by the equation:

$$R_{dp} = k_5 M_0$$

where R_{dp} is the rate of depropagation, M_0 is the concentration of the monomer, and k_5 is the rate constant of depropagation.

The rate of backbiting is given by the equation:

$$R_{bb} = k_6 M_0$$

where R_{bb} is the rate of backbiting, M_0 is the concentration of the monomer, and k_6 is the rate constant of backbiting.

The rate of chain transfer to the monomer is given by the equation:

$$R_{ctm} = k_7 M_0$$

where R_{ctm} is the rate of chain transfer to the monomer, M_0 is the concentration of the monomer, and k_7 is the rate constant of chain transfer to the monomer.

The rate of chain transfer to the polymer is given by the equation:

$$R_{ctp} = k_8 M_0$$

where R_{ctp} is the rate of chain transfer to the polymer, M_0 is the concentration of the monomer, and k_8 is the rate constant of chain transfer to the polymer.

The rate of chain transfer to the solvent is given by the equation:

$$R_{ctS} = k_9 M_0$$

where R_{ctS} is the rate of chain transfer to the solvent, M_0 is the concentration of the monomer, and k_9 is the rate constant of chain transfer to the solvent.

The rate of chain transfer to the initiator is given by the equation:

$$R_{ctI} = k_{10} M_0$$

where R_{ctI} is the rate of chain transfer to the initiator, M_0 is the concentration of the monomer, and k_{10} is the rate constant of chain transfer to the initiator.

The rate of chain transfer to the chain transfer agent is given by the equation:

$$R_{ctCA} = k_{11} M_0$$

where R_{ctCA} is the rate of chain transfer to the chain transfer agent, M_0 is the concentration of the monomer, and k_{11} is the rate constant of chain transfer to the chain transfer agent.

The rate of chain transfer to the inhibitor is given by the equation:

$$R_{ctIn} = k_{12} M_0$$

where R_{ctIn} is the rate of chain transfer to the inhibitor, M_0 is the concentration of the monomer, and k_{12} is the rate constant of chain transfer to the inhibitor.

The rate of chain transfer to the catalyst is given by the equation:

$$R_{ctCat} = k_{13} M_0$$

where R_{ctCat} is the rate of chain transfer to the catalyst, M_0 is the concentration of the monomer, and k_{13} is the rate constant of chain transfer to the catalyst.

The rate of chain transfer to the initiator is given by the equation:

$$R_{ctI} = k_{14} M_0$$

where R_{ctI} is the rate of chain transfer to the initiator, M_0 is the concentration of the monomer, and k_{14} is the rate constant of chain transfer to the initiator.

The rate of chain transfer to the chain transfer agent is given by the equation:

$$R_{ctCA} = k_{15} M_0$$

where R_{ctCA} is the rate of chain transfer to the chain transfer agent, M_0 is the concentration of the monomer, and k_{15} is the rate constant of chain transfer to the chain transfer agent.

1) **Definition:** Sei \mathcal{M} ein \mathbb{R} -Modul. Ein Element $m \in \mathcal{M}$ heißt **Nullvektor**, falls $m + n = n$ für alle $n \in \mathcal{M}$ gilt.

2) **Satz:** Sei \mathcal{M} ein \mathbb{R} -Modul. Dann existiert genau ein Nullvektor $0 \in \mathcal{M}$.

3) **Definition:** Sei \mathcal{M} ein \mathbb{R} -Modul. Ein Element $m \in \mathcal{M}$ heißt **absorptionsneutral**, falls $m + n = m$ für alle $n \in \mathcal{M}$ gilt.

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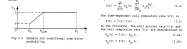
12) **Satz:** Sei \mathcal{M} ein \mathbb{R} -Modul. Dann existiert genau ein absorptionsneutrales Element $0 \in \mathcal{M}$.

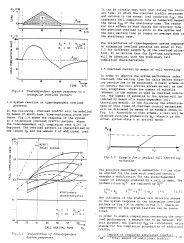
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14) **Satz:** Sei \mathcal{M} ein \mathbb{R} -Modul. Dann existiert genau ein absorptionsneutrales Element $0 \in \mathcal{M}$.

15) **Definition:** Sei \mathcal{M} ein \mathbb{R} -Modul. Ein Element $m \in \mathcal{M}$ heißt **absorptionsneutral**, falls $m + n = m$ für alle $n \in \mathcal{M}$ gilt.

16) **Satz:** Sei \mathcal{M} ein \mathbb{R} -Modul. Dann existiert genau ein absorptionsneutrales Element $0 \in \mathcal{M}$.





Die im Folgenden beschriebene Dammbauweise ist eine der neuesten und besten. Sie ist besonders für hohe Dämme geeignet, die in einem weiten Bereich der Welt gebaut wurden. Die Bauweise ist einfach und kostengünstig, und sie ermöglicht es, die Dämme in einem weiten Bereich der Welt zu bauen. Die Dämme sind aus einem besonderen Material hergestellt, das sehr stabil und langlebig ist. Die Bauweise ist auch sehr einfach zu handhaben und erfordert keine besonderen Kenntnisse. Die Dämme sind in einem weiten Bereich der Welt gebaut worden, und sie haben sich als sehr erfolgreich erwiesen. Die Bauweise ist eine der besten, die es gibt, und sie ist für alle Dämme geeignet, die in einem weiten Bereich der Welt gebaut werden sollen.



Fig. 1. Ratio of the maximum value of the function to the value of the function at the origin.



Fig. 2. Ratio of the maximum value of the function to the value of the function at the origin.

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